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APPARATUS FOR TRANSFERRING SETTLED OR SUSPENDED SOLIDS FROM  
AN OPEN VESSEL INTO A CLOSED VESSEL

5 This invention relates to apparatus for transferring  
settled or suspended solids from an open vessel into a  
closed vessel. Particularly, although not exclusively,  
this invention relates to apparatus for transferring solids  
which have been fluidised in a fluidising unit from the  
open vessel into a closed vessel at a controlled rate.

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BACKGROUND TO THE INVENTION

15 In deep sea drilling operations, huge quantities of drill  
cuttings can accumulate around a drilling rig. A growing  
awareness of the environmental impact of these drill  
cuttings has resulted in regulations requiring their  
removal and treatment. However these drill cuttings tend  
to agglomerate and are difficult to remove quickly and  
efficiently. The inventors have devised a method of  
20 fluidising settled solids, in order to cause the solids to  
form a slurry which can be removed from the sea bed for  
treatment, storage or transport. In order to improve the  
efficiency of the process, it has been proposed that once  
the drill cuttings have been fluidised, they are  
25 transported to shore or into a vessel in a continuous or  
batch process, so that the rate at which the drill cuttings  
can be removed is maximised.

30 In an alternative application, it may be desirable to drain  
a tank containing for example toxic and/or radio active  
waste with both liquid and solid constituents. For example  
it may be that the original storage tank has corroded,  
or the contents are to be removed for treatment. In this  
application, it is clearly important that the contents of  
35 the tank are contained at all times and that the volume of

material which is transferred is minimised while still providing sufficient disturbance of the solids in the tank to ensure complete suspension of the solids and controlled emptying of the tank. Alternatively, it may be desirable  
5 to remove the solids/sludge from the bottom of the tank, without overly disturbing the fine solids, and in particular without adding to or subtracting from the volume of liquid in the tank, thus ensuring that the required liquid level in the tank is maintained. This has  
10 particular relevance when the liquid level above the solids acts as a radiation shield.

#### STATEMENT OF INVENTION

15 According to a first aspect of the present invention there is provided apparatus for transferring settled or suspended solids from an open vessel into a closed vessel, the apparatus comprising a suction line which extends from the closed vessel to the open vessel via a pump or compressor  
20 and a solids feed line which extends from the solids outlet in the open vessel to a solids inlet in the closed vessel, a fluidising apparatus being provided to fluidise the solids in the open vessel.

25 The term "open vessel" is intended to encompass any vessel open to the atmosphere or to any natural open structure which contains fluid, such as a lake bed or sea bed.

Preferably, the fluidising apparatus comprises a flow  
30 chamber having a fluid inlet and a fluid outlet, means for establishing a swirling or coanda flow in a fluid passing out of the fluid outlet, and a transport outlet for transporting fluidised material away from the flow chamber. The transport outlet may be situated externally or  
35 internally of the flow chamber, and is preferably situated

on a central axis of the flow chamber. Most preferably, it is situated above the flow chamber.

- Preferably, means is provided for controlling the rate at which solids are transferred from the open vessel into the closed vessel. Preferably, these means comprise a flow meter which measures the rate of flow of suspended solids in the suction line or feed line.
- 10 Preferably, the closed vessel comprises a feed vessel which feeds suspended solids into a transport vessel containing a fluidising unit. Preferably, the transport vessel comprises a solids outlet through which suspended solids are discharged at a controlled rate along a slurry
- 15 discharge line. Preferably, means are provided on the slurry discharge line for measuring the flow rate of slurry discharge. Preferably, a bypass line is provided to allow fluid from the open vessel to bypass the fluidising unit and to pass directly into the slurry discharge line to
- 20 control slurry concentration. Preferably, a valve is provided in the bypass line. Preferably, an ultrasonic unit is disposed in the slurry discharge line to deagglomerate the slurry.
- 25 Preferably, means are provided for controlling the flow rate and/or concentration of suspended solids from the open vessel into the closed vessel based on the flow rate and/or concentration of suspended solids from the transport vessel, so that the solids content of the transport vessel
- 30 is maintained at a substantially constant level.

Preferably, the flow rate of suspended solids from the open vessel to the closed vessel and the rate of discharge of suspended solids from the transport vessel are controlled

35 by means of valves. Most preferably, the valves are

controlled by a computer, dependent on input from flow meters. Preferably, the flow meters are "density" meters or mass flow meters such as coriolis meters.

5 According to a second aspect of the present invention, there is provided a method of transferring settled or suspended solids from an open vessel into a closed vessel, the method comprising the steps of:

- 10 (a) drawing fluid from the closed vessel into the open vessel;
- (b) operating a fluidising unit to fluidise the settled or suspended solids; and
- (c) drawing the fluidised solids from the open vessel into the closed vessel.

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Preferably, the fluidising unit is driven by fluid drawn from the closed vessel.

20 Preferably, the fluid is drawn from the closed vessel into the open vessel by means of a pump or compressor.

Preferably, the fluid in the closed vessel is drawn initially from the open vessel and is recirculated between the closed vessel and the open vessel, so that no  
25 additional fluid is added to the system.

Preferably, the method further comprises the step of:

- 30 (d) controlling the rate of discharge of the fluid and fluidised solids from the closed vessel into a discharge vessel, so that the concentration of solids discharged from the discharge vessel is maintained at a predetermined rate.

35 Thus, batchwise flow can be delivered to the closed vessel from the open vessel, whilst the slurry discharge from the

discharge vessel is maintained at a constant concentration and/or flow rate.

5 Preferably, the step of controlling the rate of discharge is achieved by controlling a valve on an opening or pipe connecting the closed vessel to the discharge vessel.

10 Preferably, the method further comprises the step of fluidising the solids in the discharge vessel.

Preferably, no fluid other than the fluid in the open vessel is used to fluidise and transport the settled and suspended solids from the open vessel to the closed vessel.

15 Preferably, no fluid other than the fluid in the open vessel is used to transport the settled and suspended solids from the closed vessel to the discharge vessel.

20 The above method and apparatus can be adapted for many uses, and in particular may be used in any of the following processes:

1. A process which can operate below sea level to remove contaminated material from the seabed and hydro hoist  
25 the material to a receiving ship or barge for treatment or transportation to the shore.

2. A process for removing material from the seabed for the purpose of dredging, or the mining/retrieval of  
30 valuable elements.

3. A process for the removal of radioactive waste solids from storage ponds and tanks associated with any nuclear installations or power stations. The solids  
35 may be transported from the storage pond or tank to a

cementing or sinter process for safe containment, either during operations or during decommissioning.

4. A process for removing solids from the bottom of a  
5 mineshaft, or back filling a mineshaft. Preferably,  
the bottom of the mineshaft comprises the open vessel,  
and the closed vessel and discharge vessel as situated  
at the surface adjacent the mine shaft. Preferably, a  
supply of liquid from the surface is used to feed the  
10 closed vessel and discharge vessel, so taking  
advantage of the hydrostatic head provided by  
supplying the liquid from the surface.
5. A process in which waste from mining operations is  
15 lifted to a transport vessel at the mine base for  
hydro transportation of the waste material to back  
fill a mine.

#### BRIEF DESCRIPTION OF THE DRAWINGS

20 For a better understanding of the present invention and to  
show how it may be carried into effect, reference will now  
be made, by way of example to the accompanying drawing  
which is a schematic representation of a continuous feed  
25 and discharge system for transporting suspended solids.

#### DETAILED DESCRIPTION OF A PREFERRED EMBODIMENT

Referring to the drawing, a tank of waste 2 containing both  
30 liquid and solid constituents is to be emptied into a  
slurry discharge pipeline 4 via an intermediate vessel 6  
and a hydro transport vessel 8. Fluidising units 10, 12  
are provided in the tank 2 and hydro transport vessel 8.  
Each fluidising unit 10, 12 comprises a flow chamber 14,  
35 16 which imparts a swirling flow to fluid which is forced

into the flow chamber 14, 16 under pressure, and a discharge opening 18, 20 through which suspended solids, which have been fluidised by the fluidising units 10, 12, exit the tank 2 and hydro transport vessel 8, respectively  
5 as a controlled slurry.

A suction line 22 extends from an upper part of the intermediate vessel 6, via a pump 24 into the fluid inlet of the flow chamber 14 in the tank 2. A solids feed line  
10 26 extends from the discharge opening 18 of the fluidising unit 10 into the intermediate vessel 6 beneath an annular baffle 28. A gravity feed line 29 fitted with a valve V1 connects the bottom of the intermediate vessel 6 to the top of the hydrotransport vessel 8.

15 The fluidising unit 12 in the hydrotransport vessel 8 is supplied with water under pressure from a water tank 30 via a pump 32 and water supply line 34. The water supply line 34 passes through a lower end of the hydro transport vessel  
20 8 into the flow chamber 16 of the fluidising unit 12. The discharge opening 20 of the fluidising unit 12 is connected to the slurry discharge line 4.

A first bypass line 36 extends directly from the suction  
25 line 22 into the tank 2 and is controlled by a first bypass valve V2. A second bypass line 38 extends between suction line 22 and the solids feed line 26 and is controlled by a first computer controlled valve C1. A third bypass line 40 extends between the intermediate vessel 6 in the region of  
30 the annular baffle 28, to the upper region of the hydro transport vessel 8 and is controlled by a second computer controlled valve C2. A fourth bypass line 42 extends between the upper region of the hydro transport vessel 8 and the water supply line 34 and is controlled by a third  
35 computer controlled valve C3. Finally, a fifth bypass line

44 extends from the water supply line 34 to the slurry discharge line 4 and is controlled by a fourth computer controlled valve C4.

- 5 First and second coriolis mass flow meters 46, 48 are provided in the solids feed line 26 and slurry discharge line 4 respectively. The output from the coriolis flow meters 46, 48 is input to a computer 50 which uses control algorithms to control the degree of opening of the computer  
10 controlled valves C1 to C4.

The apparatus is designed to operate continuously, so that a continuous flow of fluidised solids is discharged at a predetermined rate down the slurry discharge line 4 after  
15 which it can be treated transported or stored as appropriate. The system operates as follows.

The intermediate vessel 6 may be vented to atmosphere prior to initiation of flow (so that the intermediate vessel 6  
20 has a cyclic flow profile). Whether or not the intermediate vessel 6 is first vented, flow is initiated by starting the pump 24, so that fluid is drawn from the intermediate vessel 6 to the tank 2 through the suction line 22. With the valves V1 and C1 fully closed, the fluid  
25 under pressure passes into the flow chamber 14 of the fluidising unit 10 and is ejected as a swirling flow, which fluidises the surrounding solids in the tank 2.

Operation of the pump 24 creates a reduction in pressure in  
30 the intermediate vessel 6 which causes the fluidised solids to be drawn into the discharge opening 18 of the solids feed line 26 and to be ejected into the intermediate vessel 6 beneath the annular baffle 28. It will be appreciated that the annular baffle 28 deflects the solids downwardly  
35 towards the bottom of the intermediate vessel 6, so that



fluid withdrawn from the top of the intermediate vessel 6 into the suction line 22 is substantially free of solids.

5 The valve V1 which connects the intermediate vessel 6 to the hydrotrans vessel 8 is opened to allow the solids in the intermediate vessel 6 to fall under gravity into the hydrotrans vessel 8. At the same time as the pump 24 is pumping fluid around the suction line 22, the pump 32 is operating to pump water from the water tank 30 into the  
10 flow chamber 16 of the fluidising unit 12. A swirling flow of fluid is discharged from the flow chamber 16 and fluidises the solids in the bottom of the hydro transport vessel 8. The entry of water under pressure into the hydro transport vessel 8 causes a positive pressure differential  
15 which forces the fluid and fluidised solids into the discharge opening 20 of the slurry discharge line 4, so that there is a constant feed of fluidised solids along the slurry discharge line 4.

20 The coriolis meter 48 measures the mass flow rate in the slurry discharge line 4 and inputs this data to the computer 50. At the same time, the coriolis flow meter 46 measures the mass flow rate in the solids feed line 26 and inputs this data to the computer 50. The computer 50 is  
25 programmed to adjust the opening of the computer controlled valves C1 to C4 so as to establish a stable relationship between the mass flow rate of the fluidised solids entering the intermediate vessel and the mass flow rate of the fluidised solids passing down the slurry discharge line 4.  
30 For example, if the mass flow rate measured by the coriolis meter 46 in the solids feed line 26 is insufficient to maintain the level of solids in the intermediate vessel 6 and hence the feed of solids to the hydro transport vessel 8, the computer 50 can operate to open the computer  
35 controlled valve C4, so that the fluidising unit 12 is less

effective and the concentration of suspended solids in the flow along the slurry discharge line 4 is reduced. Alternatively, if the mass flow rate measured by the coriolis meter 46 in the solids feed line 26 is too great, such that the solids in the hydro transport vessel 8 transferred from the intermediate vessel 6 are building up faster than they are being removed down the slurry discharge line 4, the computer 50 can operate to increase the degree of opening of the computer control valve C1, so that the fluidising unit 10 is at least partially bypassed and the concentration of suspended solids in the flow in the solids feed line 26 is reduced.

In the illustrated embodiment, the suction line 22 extends from an upper part of the intermediate vessel 6. In an alternative embodiment, the suction line 22 extends from the base of the intermediate vessel 6, drawing through a lateral collection system which is positioned within a filter media bed (not shown) below the fluidising unit 12. This arrangement could be used in a batch system or single vessel system, rather than a continuous feed system, and would be particularly effective in capturing fine slow settling solids into the slurry. In a batch system, the hydrotransport vessel 8, discharge line 4 and associated mass flow meter could be dispensed with and the solids discharged from the intermediate vessel 6 in batches. The batch discharge of solids could be controlled by the computer 50 on the basis of input from the mass flow meter 46 alone. However, other control input, such as a measurement of level of settled solids in the intermediate vessel 6 could be used to trigger batch discharge.